Optimization of Microwave Pyrolysis of Castor Oil to Sebacic Acid

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Castor oil is a widely used biomass energy source. In this paper, the process conditions for the preparation of sebacic acid by cracking castor oil using the microwave method were investigated using environmentally friendly and recyclable liquid paraffin (petrolatum) as a solvent. The optimum conditions for the reaction were determined in the experiments as follows: the mass ratio of solvent: castor oil: sodium hydroxide was 4:1:2.5 and the concentration of sodium hydroxide solution was 50% (w/t). The average microwave power was 210 W, the temperature was about 280 °C, the cracking time was 25 min under nitrogen protection, and the yield of sebacic acid was measured to be 85%. The solvents can be recycled and the recovered solvent can be used again without affecting the yield of sebacic acid. The solvent recovery was more than 92%.

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INTRODUCTION

Castor oil is a vegetable oil extracted from castor seeds, and its role as a renewable biomass energy source has been increasingly emphasized (Jeon et al. 2019; Yu et al. 2020; Becquet et al. 2021; Bhukya and Kaki 2022). Sebacic acid is also an important chemical raw material, which is widely used in the manufacture of a series of products such as fibers, engineering plastics, high-temperature lubricants, plasticizers, etc. (Jin et al. 2013; Ahmed et al. 2014; Deng et al. 2020; In et al. 2020; Thampi et al. 2023). Traditionally, sebacic acid is produced by high-temperature alkali fusion cracking of castor oil with phenol or cresol as a diluent, but there are a series of problems such as highly variable quality of the product, dark color, and difficulty to deal with a large amount of phenol-containing wastewater generated during the reaction process (Zhang et al. 2009; Xu et al. 2013; Chavhan et al. 2014; Haim-Zada et al. 2016; Yu et al. 2019; Matyszczak et al. 2020). Lu and Jiang (2005) considered microwave cracking of castor oil under the conditions of using the organic solvent 2-octanol and no solvent, respectively. With the increase of reaction temperature, the organic solvent with a low boiling point evaporates, which makes it difficult to recover the solvent. Thus, the reaction system mobility is poor, and the material is very easy to carbonize, resulting in low yields of sebacic acid (Yabalak et al. 2015; Kolyado et al. 2016; Perin and Felisberti 2022).

Castor oil was used as the raw material in this study. Cheap, non-toxic, high boiling point plant-derived alkane oil was used as solvent. The microwave cracking method was used to produce sebacic acid. Microwave heating avoids the hysteresis of heat transfer in the air medium during electrical heating, thus increasing the heating rate. Scholars

proposed the idea of microwave-cracking aviation oils (Zhang *et al.* 2022). Microwave production of sebacic acid with high yields solves the problems of difficult solvent recovery and high loss rates in other sebacic acid production methods. The solvent is insoluble in water and can be separated. The recovered solvent can be reused without affecting the sebacic acid yield and product quality.

EXPERIMENTAL

Reagents and Equipment

The reagents used were castor oil (industrial grade), liquid paraffin (petrolatum) (industrial grade, completely saturated, boiling point \geq 300 °C), sodium hydroxide (analytical pure, 99%), concentrated sulfuric acid (analytical pure, 98%), and distilled water.

Specialized equipment included an infrared spectrometer (Nicolet 5700 Nicolet Corporation, Waltham, MA, USA), nuclear magnetic resonance hydrogen spectrometer (AVANCE NEO-400MHz, Bruker, Karlsruhe, Germany), and multi-differential scanning calorimeter (DSC822e, Mettler Toledo, Columbus, OH, USA).

Fig. 1. (a) Saponification, (b) microwave cracking, and (c) acidification reactions

Reaction Principles

Saponification reaction

First, castor oil in sodium hydroxide solution underwent a saponification reaction to form glycerol and sodium ricinoleate (Fig. 1a).

Microwave cracking reaction

Next, the reaction solution was cracked at high temperature under microwave radiation, and sodium ricinoleate reacted to produce hydrogen, 2-octanol, and sebacic acid disodium salt (Fig. 1b).

Acidification reaction

Finally, the disodium salt of sebacate was acidified to form sebacic acid (Fig. 1c).

Method

Castor oil was mixed with aqueous NaOH solution under stirring, slowly heated to boiling, and then saponified under reflux for 30 minutes. At the end of saponification, the glycerol was cooled and separated. The saponified product was mixed with the solvent streptane oil under uniform stirring and then transferred to a microwave oven for radiant heating under nitrogen protection. At the end of the reaction, a certain amount of 90 °C hot water was added to the product for stirring, and at the end of the stirring, the product was put into a separatory funnel for stratification. The upper layer was the solvent phase, the middle was the unreacted oil phase, and the lower layer was the water phase. The water phase, unreacted liquid-oil phase, and solvent phase were separated sequentially. The separated unreacted liquid and solvent were washed several times with hot water. The first, second, and third washes were combined with the aqueous phase, and the rest of the washing water was stored for reuse. The aqueous phase was acidified with 3 M sulfuric acid to pH 7 at 50 °C and then left to stratify. The unreacted oil phase was separated again, and the aqueous phase was acidified with 3 M sulfuric acid to pH 2 at room temperature, and then cooled, crystallized, filtered, and dried to constant weight to obtain sebacic acid. The pH 2 filtrate was evaporated and cold crystallized, and sodium sulfate was removed and stored for reuse. The solvent recycling storage was used again.

RESULTS AND DISCUSSION

Average Microwave Output Power vs. Sebacic Acid Yield and Solvent Loss

The results of sebacic acid yield by varying the average output power of the microwave and cracking time of 25 min and by varying the mass ratio of alkali (NaOH), solvent, and castor oil of 2.5:4:1 and the alkali concentration of 50% (wt) are shown in Fig. 2. When the microwave power was low, the thermal cracking temperature was low, the temperature of the reaction system did not reach the cracking temperature and the sebacic acid yield was low. But when the temperature was low, the solvent volatilization was less and the loss rate was lower. By contrast, when the microwave power was high, the temperature of the reaction system was too high, and carbonation of the reactants occurred before they were fully cleaved to the target products, so the sebacic acid yield was low and even sebacic acid was unable to be obtained. A high reaction temperature will lead to the increase of solvent component volatilization and a high loss rate. Therefore, under the experimental conditions, the most suitable average microwave output power was 210 W.

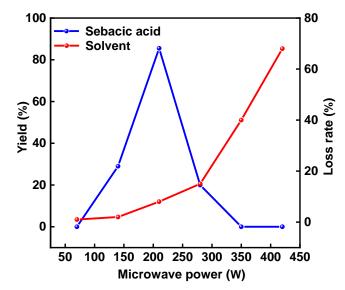


Fig. 2. Sebacic acid yield and solvent loss under different microwave average output power

The Effect of Microwave Radiation Time on the Yield of Sebacic Acid and Solvent Loss

Results are shown in Fig. 3 for an alkali concentration of 50% (wt), mass ratios of alkali (NaOH), solvent, and castor oil of 2.5:4:1, in the microwave average power of about 210 W, as a function of the microwave radiation time. When the cracking time was lower than 20 min, the reaction was incomplete, the reaction system temperature was low, the solvent volatilization was low, the loss rate was low, and the sebacic acid yield was low. When the cracking time was more than 25 min, the reaction system was carbonized due to the local overheating; the sebacic acid yield became low or even could not be recovered, and the loss rate of the solvent was also obviously increased. Therefore, the optimum reaction time was 25 min under the experimental conditions.

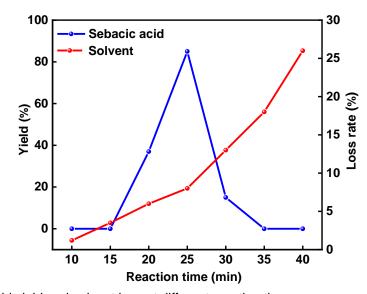


Fig. 3. Sebacic acid yield and solvent loss at different reaction times

Effect of Solvent Dosage on Sebacic Acid Yield and Solvent Loss

Figure 4 shows results for a mass ratio of alkali (NaOH)/oil (castor oil) of 2.5:1, a concentration of alkali of 50% (wt), an average microwave power was about 210 W for 25 min, and with a variable mass ratio of solvent to castor oil. When the mass ratio of solvent and castor oil was low, the reaction system had poor fluidity, and local high temperatures easily occurred during the reaction process. This resulted in the carbonization of raw materials or products, leading to a decrease in sebacic acid yield and increasing solvent loss. With the increase of the mass ratio of solvent and castor oil, the reaction system was uniformly dispersed, avoiding the local overheating phenomenon in the reaction process, and the sebacic acid yield increased. Solvent loss was reduced. The solvent and castor oil mass ratio was too high, and the reaction system was not uniformly dispersed, leading to easy settling and stratification. The intermolecular contact during the reaction was reduced, and the sebacic acid yield was reduced, such that the loss of solvent remained unchanged. Therefore, the optimum reaction condition was a single reaction under the condition of solvent: castor oil 4:1, with the lowest solvent loss and the highest sebacic acid yield.

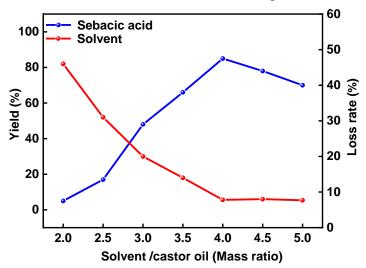


Fig. 4. The yield of sebacic acid and the loss rate of solvent under different amounts of solvent

Repeated Test for Optimum Process Conditions

The experiment was repeated three times under the conditions of alkali (NaOH), solvent, castor oil mass ratio of 2.5:4:1, average microwave output power of 210 W, cracking time of 25 min, and alkali concentration of 50% (wt). Under these conditions, the sebacic acid yields were obtained as 85.6%, 86.1%, and 86.4%, respectively, and the solvent loss rates were 8.2%, 7.6%, and 7.8%, respectively.

Exploring Solvent Recovery and Sebacic Acid Yield under Optimal Reaction Conditions

In the next series of tests the ratio of alkali (NaOH), solvent, and oil castor oil was 2.5:4:1, the average power of the microwave was about 210W, the cracking was done for 25 min, and the concentration of alkali was 50% (wt), and the number of times of solvent recycling was changed. The solvent yield increased after repeated use, and the low-boiling substances in the solvent were removed after repeated use. The recovery tended to be constant after the increase. The repeated use of solvent did not affect the sebacic acid yield.

Number of times used	1	2	3	4	5
Recovery Ratio (%)	92.5	92.5	96.6	96.8	95.8
Sebacic Acid Yield (%)	85.8	86.3	86.1	85.4	86.4

Table 1. Recoveries of Multiple Solvent Applications and Yields of Sebacic Acid

Product Characterization

Infrared spectra of synthesized products

The infrared spectrum of castor oil shows the stretching vibration peaks of -C-O at 1078.7 cm⁻¹ and -COOR at 1171.5 cm⁻¹, the absorbance peaks of C=C at 1146.1 cm⁻¹, and the peaks of -C=O at 1742.5 cm⁻¹, and the peaks of -OH at 3401.1 cm⁻¹. It can be seen that the stretching vibration peaks of C=C and -COOR at 1146.1 cm⁻¹ and 1171.5 cm⁻¹ were converted during the reaction. This confirms that the castor oil had reacted.

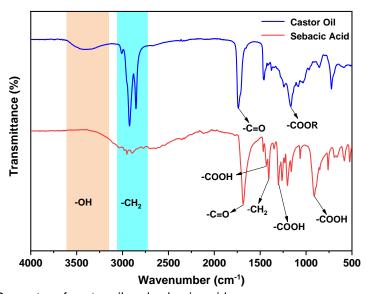


Fig. 5. IR spectra of castor oil and sebacic acid

In the infrared spectrum of sebacic acid, 911.1 cm⁻¹ is the out-of-plane bending vibration of -OH in the sebacic acid dimer, 1299.9 cm⁻¹ is the bending vibration characteristic absorption peak of -COOH in sebacic acid, 1407.1 cm⁻¹ is the shifting vibration peak of -CH₂, and 1685.2 is the stretching vibration peak of -C=O. The wavenumbers 2802.5 and 3330.7 cm⁻¹ correspond to the bending vibration peaks of -CH₂ and -OH, as well as the -CH₂ and -OH stretching vibration peaks. The infrared spectra of the products prepared by this method were consistent with the positions of the main characteristic peaks in the standard spectra of sebacic acid.

Infrared spectra of saponification by-products

Figure 6 shows the infrared spectrum of the by-product glycerol, in which the -OH stretching vibration peak is at 3327.6 cm⁻¹. The stretching vibration peak at 1038.8 cm⁻¹ is the -C-O bond, and the -O-H bending vibration peak is at 1419.5 cm⁻¹.

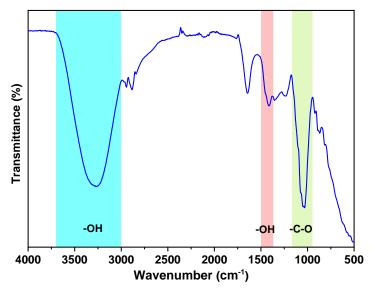


Fig. 6. Infrared spectrum of by-product glycerin

Thermal analysis

The results were measured with a differential scanning calorimeter, as shown in Fig. 7. The melting point of the synthesized product sebacic acid was 131 °C, which is consistent with the melting point of sebacic acid.

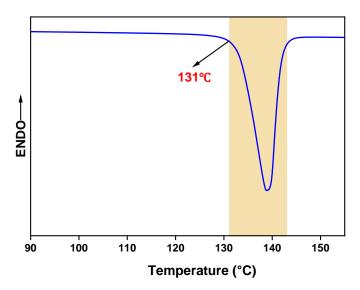


Fig. 7. DSC curve of product sebacic acid

To further determine the generation of sebacic acid, the product was analyzed using an NMR hydrogen spectrometer with methanol as the deuterium substituting reagent; the results are shown in Fig. 8. Results were as follows: ^{1}H NMR (400 MHz, methanol-d4) δ 2.27 (t, J = 7.4 Hz, 4H), 1.60 (t, J = 7.3 Hz, 4H), 1.33 (m, 8H). The NMR hydrogen spectrum analysis indicated that the product was sebacic acid.

In sum, this process is more in line with the concept of green chemistry. The use of liquid paraffin (petrolatum) as a solvent for microwave cracked castor oil to produce sebacic acid improves the yield and quality of sebacic acid. Further exploration into the production of sebacic acid is required.

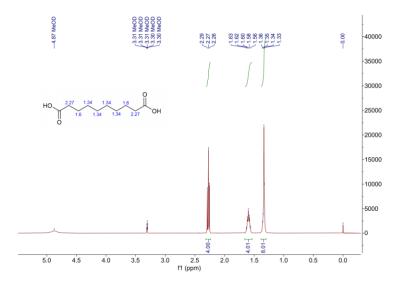


Fig. 8. ¹H NMR diagram of product Sebacic acid

CONCLUSIONS

- 1. The traditional industrial production method of sebacic acid is to use phenol or cresol as a solvent to crack castor oil by high-temperature alkali fusion. The average cracking time of the traditional method is 3 to 5 h, with high energy and time consumption, and the production of one tonne of sebacic acid produces 20 to 30 t of phenol-containing wastewater, which is difficult to treat. In contrast, the sebacic acid production method in this study is simple and greatly reduces the reaction time and energy consumption. It also reduces the generation of wastewater and reduces the damage to the environment during the production process.
- 2. When using the new method, the product sebacic acid yield can reach 85%. As a solvent of liquid paraffin (petrolatum) is safe, non-toxic, and easy to recycle. The recovery rate is more than 92%, and multiple uses do not affect the sebacic acid yield.

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